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ORTHOGONAL COLLOCATION SIMULATION OF THE ROTATING DISC ELECTROD—ETC((I)
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Orthogonal Collocation Simulation of the Rotating Disc Electrode

Ву

Bernd Speiser, Stanley Pons and Jerome McAleer

Prepared for Publication in Electrochimica Acta

University of Alberta Department of Chemistry Edmonton, Alberta, Canada T6G 2G2



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REPORT DOCUMENTATION PAGE 40-4118712 12 (and Submitted Orthogonal Collocation Simulation Rotating Disc Electrode Technical Report # 12 PERFORMING ONG. REPORT CONTRACT OF CHART BURSERY Stanley Pons, Bernd Speiser, and J. McAleer N00014- 82-G-0017 M. PROLING ELEMENT PROJECT, TASK SEANCE CHE BRAN WOLFE SING DRING TO STAND IN ST Department of Chemistry University of Alberta Edmonton. Alberta, Causda TeG 2G2 Confeding Office went and adopted Task No. NR 359-718 Office of Naval Research
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16. SECURITY CLASS (NO MIG.) SENE DULE 16 East Redu from STATEMENT (of min Report) This document has been approved for public release and sale; its distribution unlimited. 17. DESTRIBUTION STATEMENT OF the obstock motored in Stone M. W. Sillinger Sound Electrochemistry, Simulation, Orthogonal Collocation, Rotating Disc Electrodes The theory of orthogonal collocation as applied to rotating disc systems is presented and its advantages are described. The technique is extremely fast and application of chemical reactions is easily implemented.

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ABSTRACT

The hydrodynamic problem of the rotating disc electrode is approximated using the weighted residual technique of orthogonal collocation. Results are given for a potential step applied to the electrode where simple reversible charge transfer to a single species takes place.

ORTHOGONAL COLLOCATION SIMULATION OF THE ROTATING DISK ELECTRODE

Stanley Pons⁴, Bernd Speiser, and
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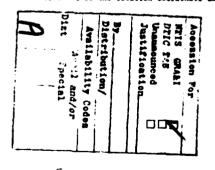
Analytical solutions for the current at rotating disc electrides (RDE) (Figure 1) are known for only the simplest electrochemical reaction mechanisms or electrical perturbations. Orthogonal collocation solution techniques, like finite difference approaches, give a single mathematical method for approximating virtually all electrochemical responses and mechanisms. The RDE is described by a partial differential equation containing square distance terms. It is shown that such non-linearity presents no special problems in the approximation technique. The results for the RDE are available from changing only 2 program steps in the general program solving a simple electron transfer mechanism at a stationary planar electrode.

DIMENSIONAL ANALYSIS

The general differential equation describing mass transport to a rotating disc electrode is given by

$$V_{\Gamma} = \frac{4c_1}{4c} + \frac{V_{\phi}}{c} = \frac{4c_1}{40} + V_{\phi} = \frac{4c_1}{4c}$$
 (1)

where the c_i are the concentrations of electroactive species, t is the time, z is the distance coordinate normal to the electrode surface, D_i are the diffusion coefficient, r is the distance coordinate parallel to the electrode surface, the V_i are velocity components of the fluid, and e is the rotation coordinate about





the z axis.

In the assumption of an ideal hydroghamic model, there is no change in concentration in the 0 direction. Also, we assume that V_Z is independent of r, which implies a uniform flow. We can thus approximate $\delta c/\delta r=0$ over the whole electrode when the radius of the electrode is small with respect to the sheath.

The assumptions reduce the differential equation to the

$$\frac{4c}{4c} = \frac{6^2c}{4z^2} - \frac{v_z}{4z} = \frac{4c}{4z}$$
(2)

The velocity term $\mathbf{V_Z}$ has been given by Levitch (1) and is a function of the kinematic viscosity \mathbf{v} and the rotation velocity \mathbf{w} :

$$V_{x} = -0.51 \text{ m}^{3/2} \text{v}^{-1/2} \text{g}^{2} = \text{Kz}^{2}$$
 [3]

Thus

$$\frac{6c}{4t} = \frac{6^2c}{4z^2} - \frac{6c}{4z}$$
(41)

We require to have the equation in dimensionless form. We choose as the distance coordinate

where L is a distance along the s axis where, during the time

frame of the experiment, no diffusion effects are present. We choose the time coordinate as

$$T = \frac{Dt}{L^2} \tag{6}$$

and a dimensionless constant

$$g = \frac{RL^3}{D} \tag{71}$$

Concentration is made dimensionless by dividing by the bulk concentration $c^{\hat{\boldsymbol{b}}_1}$

Substitution of [5], [6], and [8] into the differential equation [2] yields:

OF

$$\frac{4c^4}{4T} = \frac{8^2c^4}{82^2} - \frac{RL^3}{D} \times \frac{3c^4}{42}$$
[10]

$$\frac{4c^{*}}{67} = \frac{6^{2}c^{*}}{62^{2}} = 62^{2} - 62^{2}$$

$$62$$
(11)

We consider the transient current at the rotating electrode

when a potential step is applied which drives the surface concentration of the electroactive species to zero.

$$c^{*}(\theta,T) = 0$$
 $c(1,T) = 0$ (12)

It has been shown that the weighted residual method of orthogonal collocation can furnish accurate solutions to differential equations (2-4) at certain distance points in solution. The points correspond to the roots or zeros (collocation points) of orthogonal shifted Jacobi polynomials.

DISCRETIZATION OF THE DIFFERENTIAL EQUATION

The 2 differentials are discretized in terms of collocation coefficients (3):

$$\frac{dc^{\bullet}}{dz} \begin{vmatrix} & \frac{N+2}{z} \\ z_{1} & j_{-1} \end{vmatrix} A_{ij} c^{\bullet}(z_{j}, T)$$
(13)

and

$$\frac{d^{2}c^{4}}{dz^{2}}|_{z_{1}} = \frac{N+2}{j-1}B_{1j}e^{4}(z_{j},T)$$
 (14)

where \mathbf{z}_i are the roots of the Jacobi polynomial of order R chosen, and the \mathbf{A}_{ij} and \mathbf{B}_{ij} are elements of matrices given in terms of the \mathbf{z}_i only:

$$\bar{x} = \begin{bmatrix} \frac{dz_1}{dz_1} \\ \frac{dz_2}{dz_1} \end{bmatrix}$$
 (15)

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 $B = \left| \frac{d^2z_1}{dz_1^2} \right| \cdot \overline{Q}^{-1}$

The values of each of these matrix elements are easily calculated by matrix multiplication and inverse matrix routines (such as those based on Gauss-Jordan elimination) (4).

Substitution of the discretized differentials into $\{11\}$ yields:

We have now N+2 equations (2=0 and 2=1 plus the N central roots) in N+2 unknown $c^0(2_j,T)$. The dimension is reduced by two, and the problem specified to final form by introducing into (18) the known boundary conditions

$$c^{*}(0,t) = 0$$
 (19) $c^{*}(1,T) = 1$

which are the first and last terms of each summation:

$$\frac{dc^{\circ}}{dT} \bigg|_{Z_{1}} = B_{1,1} c^{\circ}(0,T) + B_{1,N+2} c^{\circ}(1,T) + \prod_{j=2}^{N+1} B_{1j} c^{\circ}(Z_{j},t) =$$

$$8Z_{1}^{2} \left[A_{1,1} c^{\circ}(0,T) + A_{1,N+2}(1,T) + \prod_{j=2}^{N+1} A_{1j} c^{\circ}(Z_{j},T) \right]$$
[20]

to yield

$$\frac{dc^{*}}{dT} \Big|_{Z_{\hat{1}}} = B_{\hat{1},N+2} + \sum_{j=2}^{N+1} B_{ij}c^{*}(Z_{j},T) - \frac{1}{2} \left[A_{\hat{1},N+2}(1,T) + \sum_{j=2}^{N+1} A_{ij}c^{*}(Z_{j},T)\right]$$

$$= \frac{3}{2} \left[A_{\hat{1},N+2}(1,T) + \sum_{j=2}^{N+1} A_{ij}c^{*}(Z_{j},T)\right]$$
[21]

Thus the concentration profiles as a function of time are readily and efficiently generated by integrating the N sets of first order differential equation [21]. One may use available subroutines from software libraries such as IMSL or SSP, or more specialized programs taking the stiffness of the differential equations into account (2,4).

As has been shown previously, more complicated mechanisms may be readily incorporated into the equations (3,4) as well as a variety of electrochemical techniques, electrode geometries (5-8), and edge effect considerations (9,10).

RDE CURRENT

Current to the RDE is given by the flux at the surface:

$$i = nFAD \left(\frac{\delta C}{\delta Z}\right)$$
 [22]

or in terms of the dimensionless concentration [8] and distance (51.

$$i = \frac{nFADc^b}{L} \left(\frac{\delta c^a}{62}\right)_{2=0}$$
 [23]

$$j = \frac{nFAD^{2/3}c^{b}K^{1/3}}{g^{1/3}} \left(\frac{4c^{+}}{62}\right)_{2=0}$$
 [24]

which is given immediately during the simulation at each time

$$i = nFAD^{2/3}c^{b}R^{1/3}s^{-1/3}\left[A_{1,N+2} + \frac{N+1}{2}A_{1,j}c^{*}(z_{j},T)\right]$$
 [25]

since the term in brackets is the dimensionless flux in equ ion [24] at 2=0 by equation [13].

We can compare our result to a series solution () which states that the time dependent current is proportional to

$$1 + 2 \sum_{m=1}^{\infty} \exp(\frac{-m^2 k^2 D t}{\delta_m^2})$$
 [26]

$$\theta_0 = 1.61 \text{ p}^{1/3} \text{w}^{-1/2} \text{v}^{1/6}$$
 (27)

Introducing the dimensionless time variable [4] into[24] we find the current is proportional to ...

1 + 2.
$$r = \exp\{-\frac{1}{2}hn^2 s^{2/3}T\}$$
= 1 (28)

, so that the ratio of the current calculated from equation [25] to the expression [28] should be Table 1. It is seen that for only aix collocation points, the current values are accurate to 0.05%. This value may be further decreased by forcing higher accuracy in the integrations (2) or increasing the number of collocation points, although ten points do not exhibit significant improvement over nine. The maximum relative error decrease using ten instead of nine collocation

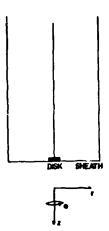
The results for the rotating ring disc electrode are being optimized, and will be the aubject of a forthcoming publication.

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Table 1. Ratio of simulated flux to analytical current-time function (Ref. 11) Beta = 10^{-1} . For typical rotation speeds (10G0 RPM), viscosities, and diffusion coefficients, the real total time simulated in the table is t = 100 ms.



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